

[CONTRIBUTION FROM THE NATIONAL ADVISORY COMMITTEE FOR AERONAUTICS AIRCRAFT ENGINE RESEARCH LABORATORY]

The System Cyclopentane-Neohexane-Aniline

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The possibility of the purification of commercial cyclopentane by extraction with aniline led to the investigation of the ternary system cyclopentane-neohexane-aniline. Analysis of the commercial hydrocarbon mixture based on physical constants showed neohexane to be the only contaminant. This was in agreement with the assumption made

tion by fractional distillation.² The use of aniline as a solvent for similar hydrocarbon mixtures has been previously described.^{3,4}

Experimental

Materials

Commercial Cyclopentane.—Purchased from Phillips Petroleum Company. Fractionation of the material on a 50-theoretical plate column gave very little separation of the impurity. The material used in the determination of the phase diagrams was distilled through a 12-inch Vigreux column. The physical constants were identical with those of the original material: n_D^{20} 1.4029, d_4^{20} 0.7364; literature values for pure cyclopentane, n_D^{20} 1.4064, d_4^{20} 0.7454.²

Neohexane.—Obtained from the same source and triply distilled before use; n_D^{20} 1.3691 and d_4^{20} 0.6501, indicating a reasonable degree of purity; literature constants, n_D^{20} 1.3688 and d_4^{20} 0.6492.²

Aniline.—J. T. Baker C. P. material was used which, after distillation, had the values n_D^{20} 1.5858 and d_4^{20} 1.0228.

Method

Commercial cyclopentane and neohexane were mixed in various proportions. The refractive index and specific gravity values of the mixtures are shown in Fig. 1. The latter values for

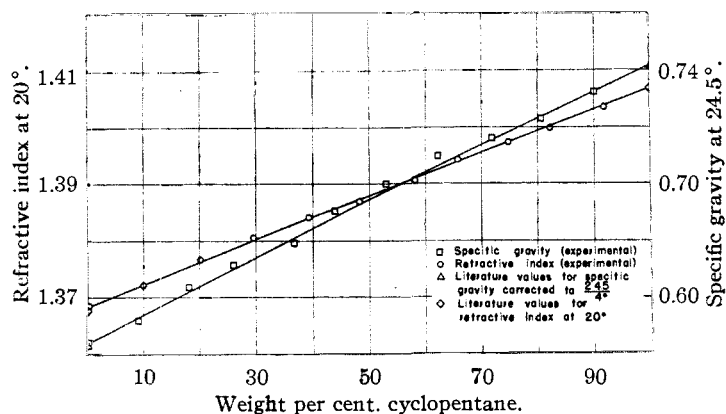


Fig. 1.—Variation of specific gravity and refractive index with weight per cent. cyclopentane in mixtures with neohexane at 24.5°.

by Tooke who investigated similar material.¹ The proximity of the boiling points of these two hydrocarbons eliminated the feasibility of purifica-

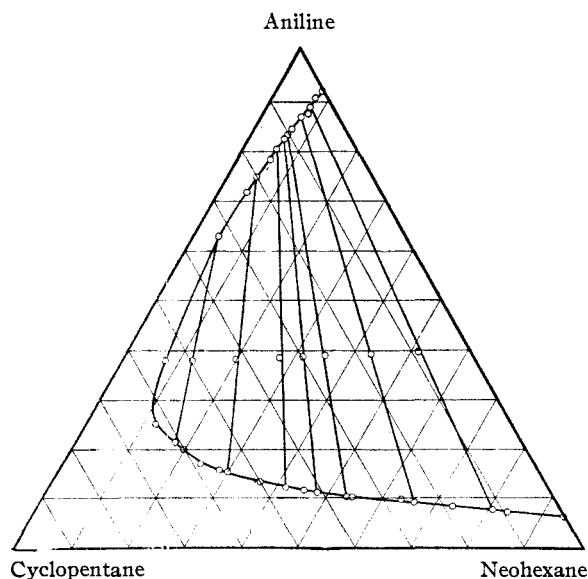


Fig. 2.—Solubility and composition of conjugate liquids (weight percentage) for the system cyclopentane-neohexane-aniline at 25°.

(1) Tooke, *Ind. Eng. Chem.*, **35**, 992 (1943).

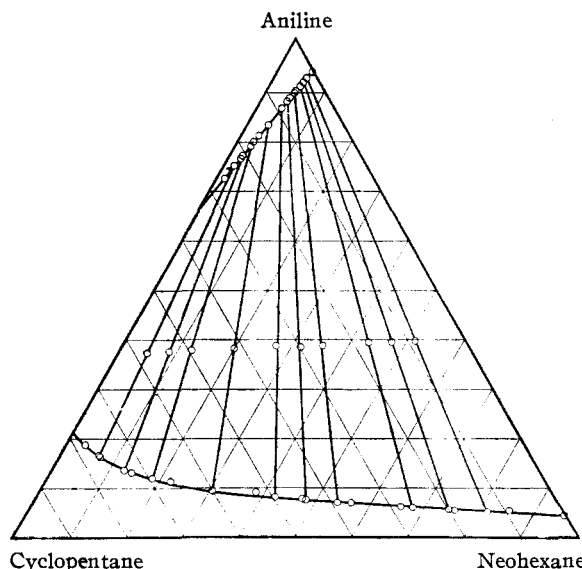


Fig. 3.—Solubility and composition of conjugate liquids (weight percentage) for the system cyclopentane-neohexane-aniline at 15°.

(2) Doss, "Physical Constants of the Principal Hydrocarbons," 4th ed., The Texas Company, New York, N. Y., 1943, pp. 1, 110.

(3) Varteressian and Fenske, *Ind. Eng. Chem.*, **29**, 270 (1937).

(4) Darment and Winkler, *J. Phys. Chem.*, **47**, 442 (1943).

the pure hydrocarbons were corrected to 24.5°.^{5,6} Calculations were then made using these data in order to determine the composition of the commercial hydrocarbon.

Mixtures of known weight ratios of cyclopentane and neohexane were made up and placed in large test-tubes in a thermostated water-bath with a temperature control of $\pm 0.05^\circ$. Aniline was then added with stirring from a water-jacketed buret at the same temperature. The amount of aniline used in each titration to the point of turbidity fixed the lower portion of the two-phase boundary of the phase diagram (Figs. 2 and 3). Similarly, known weights of aniline were placed in the test-tubes and mixtures of known weight ratios of cyclopentane and neohexane were added to obtain turbidity. The amount of hydrocarbon used fixed the upper portion of the two-phase boundary. Refractive indices were taken of the resulting mixtures at 25° in the case of the 25° diagram and at 20° in the case of the 15° diagram. When plotted against appropriate composition parameters, these indices serve to identify the composition of the top and bottom layers in the mixtures made up to determine the tie lines.

The data, as expressed by the tie lines, were obtained by selecting three-component mixtures whose compositions are shown by the points in the two-phase region. The mixtures were held at constant temperature for seventy-two hours with occasional agitation.

The data for the solubility curves and the compositions of conjugate liquids are shown in Tables I and II.

TABLE I

SOLUBILITY DATA AND THE COMPOSITION OF CONJUGATE LIQUIDS AT 25°

Hydrocarbon layer (weight per cent.)		Refractive index, n_D^{25}	Solvent layer (weight per cent.)		Refractive index, n_D^{25}
Cyclo- pentane	Neo- hexane		Cyclo- pentane	Neo- hexane	
Solubility Data					
0.0	93.8	1.3765	0.0	8.1	1.5646
9.5	83.5	1.3812	1.9	7.5	1.5625
18.5	73.3	1.3861	4.8	7.5	1.5562
27.0	63.2	1.3903	6.5	6.8	1.5528
35.3	54.4	1.3954	8.9	6.5	1.5498
43.0	45.4	1.4006	16.3	5.5	1.5355
50.1	36.8	1.4068	23.7	4.7	1.5272
55.9	28.2	1.4124	32.4	4.6	1.5187
58.6	24.2	1.4162			
60.0	19.9	1.4212			
60.6	15.8	1.4268			
62.3	12.3	1.4332			
54.5	7.7	1.4550			

Composition of Conjugate Liquids (extremities of tie lines)

0.0	93.8	1.3765	0.0	8.1	1.5646
11.9	80.5	1.3824	3.7	7.1	1.5581
25.1	65.9	1.3892	6.4	6.7	1.5531
36.3	53.4	1.3960	10.3	6.1	1.5460
40.9	48.0	1.3988	11.7	5.9	1.5437
45.7	42.0	1.4027	13.9	5.6	1.5413
54.6	30.0	1.4113	20.0	4.9	1.5321
60.8	17.7	1.4238	32.5	4.5	1.5188

Results and Discussion

The refractive index and specific gravity values of the mixtures shown in Fig. 1 were found to be linear with respect to composition. The extrapolated value for cyclopentane agreed with the

(5) Egloff, "Physical Constants of Hydrocarbons," Vol. I, Reinhold Publishing Corporation, New York, N. Y., 1939, p. 38.

(6) Egloff, *ibid.*, Vol. II, 1940, p. 54.

TABLE II

SOLUBILITY DATA AND THE COMPOSITION OF CONJUGATE LIQUIDS AT 15°

Hydrocarbon layer (weight per cent.)		Refractive index, n_D^{15}	Solvent layer (weight per cent.)		Refractive index, n_D^{15}
Cyclo- pentane	Neo- hexane		Cyclo- pentane	Neo- hexane	
Solubility Data					
0.0	95.9	1.3770	0.0	6.1	1.5705
9.7	85.1	1.3815	0.7	6.0	1.5697
19.1	75.4	1.3857	1.5	5.9	1.5685
28.1	65.8	1.3898	2.4	5.7	1.5664
36.7	56.5	1.3939	3.6	5.5	1.5642
45.0	47.4	1.3982	4.9	5.1	1.5632
52.3	38.4	1.4030	6.7	4.9	1.5588
60.0	30.3	1.4071	9.0	4.5	1.5554
66.5	22.0	1.4128	11.0	3.7	1.5522
72.4	14.3	1.4179	15.8	3.1	1.5435
76.7	6.9	1.4251	18.5	2.6	1.5382
77.9	3.2	1.4302	21.7	2.0	1.5320
			26.4	1.1	1.5246

Composition of Conjugate Liquids (extremities of tie lines)

0.0	95.9	1.3770	0.0	6.1	1.5705
13.5	81.5	1.3830	1.7	5.6	1.5678
19.9	74.7	1.3859	2.7	5.5	1.5660
26.2	67.9	1.3888	3.7	5.3	1.5641
39.0	54.0	1.3951	5.4	4.9	1.5611
44.1	48.2	1.3978	7.3	4.5	1.5575
49.3	42.5	1.4015	8.9	4.3	1.5555
60.0	30.3	1.4080	13.0	3.7	1.5470
69.4	18.5	1.4150	17.5	2.8	1.5400
73.4	12.8	1.4195	20.9	2.1	1.5340
76.5	7.1	1.4245	23.4	1.4	1.5298

literature value for the pure hydrocarbon. The assumption that the impurity was largely neohexane was thereby substantiated. The calculated composition of the commercial hydrocarbon using these data gave identical results using either the refractive index or the specific gravity value, namely, 91.8% cyclopentane and 8.2% neohexane by weight. These values were used in the calculation of composition of all known mixtures in the determination of the phase diagrams.

The refractive indices of the two phases corresponding to the ends of the tie lines were found to be in agreement within experimental error with those determined for the turbid boundary mixtures of known composition. The β values³ for this system representing the ratio of cyclopentane to neohexane in the extract layer to the same components in the raffinate layer were 2.37 ± 0.14 at 25° and 1.68 ± 0.15 at 15°.

Summary

The ternary system cyclopentane-neohexane-aniline has been investigated experimentally at 25 and 15°. Data for the solubility curves and the composition of conjugate liquids and the phase diagrams are given.